

## Model for thermal conductivity of CNT-nanofluids

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**Abstract.** This work presents a simple model for predicting the thermal conductivity of carbon nanotube (CNT) nanofluids. Effects due to the high thermal conductivity of CNTs and the percolation of heat through it are considered to be the most important reasons for their anomalously high thermal conductivity enhancement. A new approach is taken for the modeling, the novelty of which lies in the prediction of the thermal behaviour of oil based as well as water based CNT nanofluids, which are quite different from each other in thermal characteristics. The model is found to correctly predict the trends observed in experimental data for different combinations of CNT nanofluids with varying concentrations.

**Keywords.** Thermal conductivity; nanofluid; carbon nanotube (CNT); nano-suspension; heat transfer.

### 1. Introduction

The trend of miniaturization has prompted heat transfer engineers to look for newer and innovative techniques for efficient cooling. Nanofluids are one of the potential technologies for heat transfer in future. The stable suspensions of nanoparticles (typically <100 nm) in liquids are called nanofluids; whereas suspension of carbon nanotube (CNT) in the liquid is called CNT nanofluid. Nanofluids are found to have very stable suspensions, without substantial sedimentation for a long time. They are found to eliminate most of the problems arising with slurries like sedimentation, clogging of small channels, erosion, excessive pressure drop etc. Moreover, the heat transfer capabilities of nanofluids are much enhanced as compared to base fluids. This makes them suitable for use in cooling of electronic equipments, lasers, fuel-cells, car radiators etc. The enhancement in thermal conductivity of nanofluids is unusually high and cannot be predicted by any of the conventional multiphase conductivity models like that of Maxwell–Garnett (1904). CNT nanofluids are found to be most effective in this regard, giving two orders of magnitude higher thermal conductivity enhancement compared to the usual slurries.

The greatest enhancement of thermal conductivity was observed in a subsequent study performed at ANL by Choi *et al* (2001). The nanofluid of multiwalled carbon nanotubes (MWCNTs) suspended in engine oil showed a phenomenal 150% increase in thermal conductivity with just 1% volume fraction of the nanotubes. This sudden jump in enhancement is interesting. With polymer nanotubes, similar enhancement was reported by Biercuk *et al* (2002). The reason for the abnormal rise of enhancement

is yet to be explained but one can look at two facts. Firstly, the thermal conductivity of carbon nanotubes is very high (~2000 W/mK) and secondly, the nanotubes have a very high aspect ratio (~2000). We shall indicate the implications of the aspect ratio of the nanotubes when we consider the possible theories of thermal conductivity of nanofluids.

Assael *et al* (2005) measured thermal conductivity of multi walled as well as double walled CNTs. Thermal conductivity of MWCNTs of around 130 nm average diameter and 40  $\mu\text{m}$  average length was found to be 34% for 0.6% volume whereas that of double walled CNTs was found to be 8% for 1% volume suspension in water. Hwang *et al* (2006) also obtained similar results for MWCNT suspensions in water as well as ethylene glycol. Liu *et al* (2005) also measured thermal conductivity of MWCNTs of 20–50 nm in diameter. They observed an increase of 12.4% in the thermal conductivity of CNT suspension in ethylene glycol for 1% volume fraction whereas 30% enhancement in the CNT suspension in synthetic oil for 2% volume fraction.

In the last few years, attempts have been made to model the enhancement in thermal conductivity of CNT nanofluids by various assumptions like liquid layering, fractal theory etc. Xue (2005) modelled the thermal conductivity of CNT nanofluids using field factor approach, with a depolarization factor and an effective dielectric constant. The model is found to be working fairly well in predicting the thermal conductivities of CNT suspensions. Nan *et al* (2003) presented a simple formula for thermal conductivity enhancement in CNT composites which is derived from the Maxwell–Garnett (1904) model by the effective-medium approach. The model over-predicts the enhancement in the thermal conductivity of CNT suspensions when calculated with typical values of CNT thermal conductivities. Nan *et al* (2004) also developed a

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new model by incorporating interface thermal resistance with an effective-medium approach. However, the model needs the thermal resistance value at the surface of CNTs, which is difficult to get for different types of CNTs and their combinations with different solvents. Recently, Gao and Zhou (2006) presented another model, based on differential effective medium theory, derived from the Maxwell–Garnett (1904) model. The model suggests a non-linear dependence of thermal conductivity of CNT nanofluids over volume concentration of the nanotubes, with slow increase at low concentrations and rapid at high concentrations.

There are some more models for the prediction of thermal conductivity of CNT nanofluids, but none of them conform to the experimental observations, for all the available experimental results.

The current work presents a model which will predict the thermal conductivity of CNT nanofluids. The existing model by Hemanth *et al* (2004), which predicts thermal conductivity of nanoparticles suspension, is improved here by removing the adjustable parameter used there. Two parallel paths of heat flow are considered viz. one through the conduction by liquid particles and another through the conduction by CNTs. Even at a very low volume fraction (1–2%) of the CNTs, a continuous network of the CNTs is possible due to the very small diameter and very high aspect ratio. A TEM image of these nanofluids, as seen in figure 1, indicates that the CNTs are in a random network indeed. The four orders of magnitude high thermal conductivity of CNTs is the most significant contributor in the total heat transfer through the CNT nanofluid. The model is validated against available experimental data, for different base liquids.

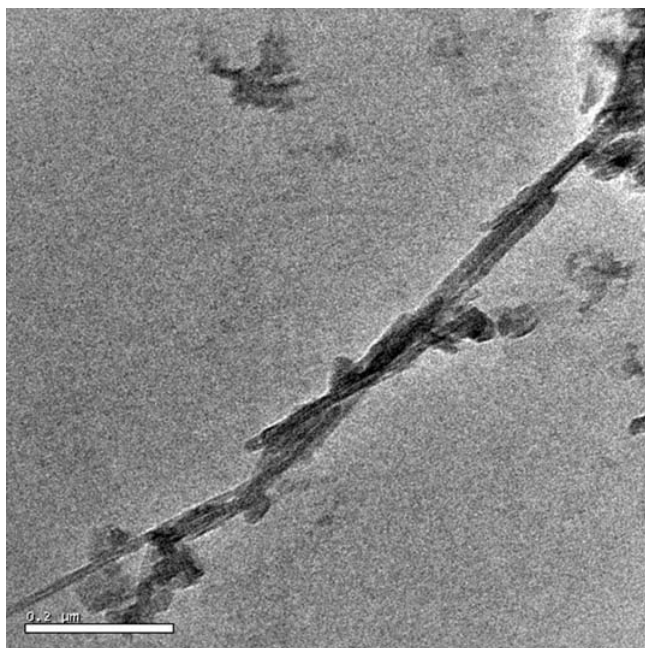


Figure 1. TEM image of CNTs.

## 2. Present model

The present model for thermal conductivity of CNT nanofluids is derived from Hemanth *et al* (2004), which is given for nanoparticle suspensions. The model considers two paths for heat to flow in a CNT nanofluid. One through the base liquid and the other one through the CNTs. These two paths are assumed to be in parallel to each other. Thus, two continuous media are considered here, participating in the conductive heat transfer. Usually, the aspect ratio of CNTs is very high (around 2000) and hence, a continuous net of CNTs available for heat transfer is a valid assumption. Thus, total heat transfer through nanofluid can be expressed as

$$q = q_1 + q_s, \quad (1)$$

$$q = -k_1 A_1 \left( \frac{dT}{dx} \right)_1 - k_s A_s \left( \frac{dT}{dx} \right)_s, \quad (2)$$

where  $A$ ,  $k$ ,  $(dT/dx)$  denote the heat transfer area, thermal conductivity and temperature gradient of the respective media. Subscripts, 1 and s, denote quantities corresponding to the liquid medium and solid CNT medium, respectively. The liquid medium and the CNTs are assumed to be in local thermal equilibrium at each location, which gives

$$\left( \frac{dT}{dx} \right)_1 = \left( \frac{dT}{dx} \right)_s = \left( \frac{dT}{dx} \right). \quad (3)$$

Thus, (1) can be written as

$$q = -k_1 A_1 \left( \frac{dT}{dx} \right) \left[ 1 + \left( \frac{k_s A_s}{k_1 A_1} \right) \right]. \quad (4)$$

Hemanth *et al* (2004) derived the expression for thermal conductivity enhancement in nanoparticle suspensions denoting the liquid and solid particle radii to be  $r_1$  and  $r_s$  as well as volume fraction of the nanoparticles as  $\varepsilon$  and the volume fraction of the liquid as  $(1 - \varepsilon)$ .

$$q = -k_1 A_1 \left( \frac{dT}{dx} \right) \left[ 1 + \frac{k_s \varepsilon r_1}{k_1 (1 - \varepsilon) r_s} \right] = -k_{\text{eff}} A_1 \left( \frac{dT}{dx} \right), \quad (5)$$

where the effective thermal conductivity is expressed as

$$k_{\text{eff}} = k_1 \left[ 1 + \frac{k_s \varepsilon r_1}{k_1 (1 - \varepsilon) r_s} \right]. \quad (6)$$

The rate of heat transfer can be expressed in dimensionless form as

$$q^* = \frac{q}{-k_1 A_1 \left( \frac{dT}{dx} \right)} = 1 + \frac{k_s \varepsilon r_1}{k_1 (1 - \varepsilon) r_s} = \frac{k_{\text{eff}}}{k_1}, \quad (7)$$

where the numerator represents the rate of heat transfer of the nanoparticle suspension, and the denominator is the rate

of heat transfer in the absence of nanoparticles. However, Hemanth *et al* (2004) did not explain the term  $r_1$ , i.e. liquid particle size. It was left as an undefined parameter and for the purpose of calculation, it was accommodated in the constant 'c' used in next step of the model.

Here, we use the same expression (7) as derived by the stationary particle method developed by them for calculating the effective thermal conductivity of CNT nanofluids. The  $r_1$  is taken as liquid molecular size and  $r_p$  as average diameter of the suspended CNTs. The application of this model with above assumptions and definitions is presented here for predicting the thermal conductivity enhancement of CNT nanofluids.

### 3. Results and discussion

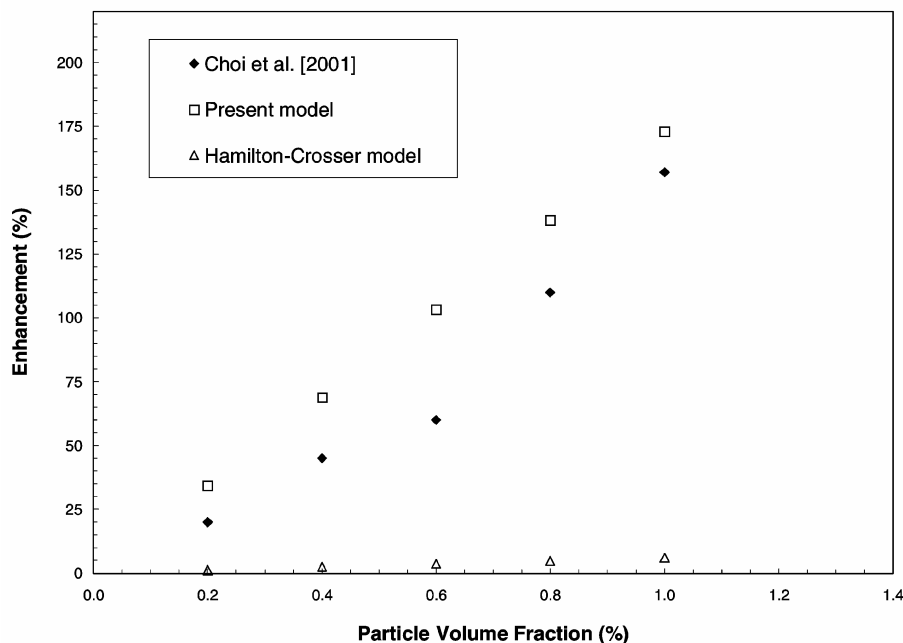
The model shows linear dependence on CNT volume concentration and inverse dependence on the CNT diameter. Figure 2 shows the comparison of the model with the experimental data of Choi *et al* (2001). The enormous enhancement in the thermal conductivity of multiwalled CNT in oil nanofluid at very low volume fractions is predicted by the model very well. The average size of the multiwalled CNTs used is 25 nm in diameter and 50  $\mu\text{m}$  in length with around 30 annular layers. The experiments show an enhancement of 157% at just 1% medium and the Hamilton–Crosser (1962) model fails completely to predict such a high enhancement.

Also, the experimental data shows the linear dependence of CNT concentration on the effective thermal volume of the CNTs and 45% enhancement at 0.4% volume

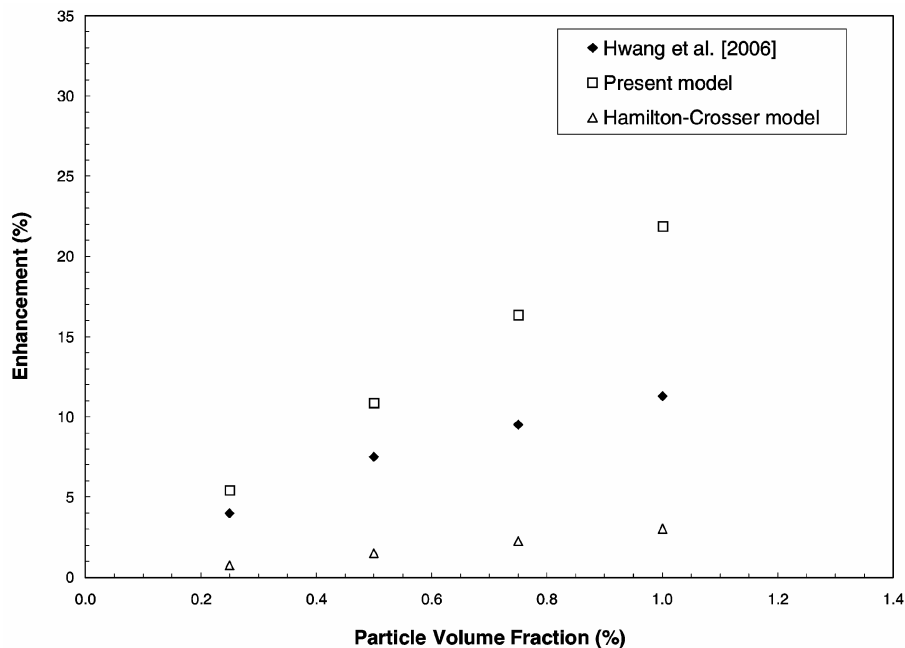
concentration. The classical model for solid medium suspended in liquid medium conductivity of nanofluid is predicted well by the model. The liquid particle size for the oil used for calculations is 3.1  $\text{\AA}$ . Figure 3 shows the comparison of the model with the experimental data of Hwang *et al* (2006). The experiments show that the multiwalled CNTs suspended in water show quite less enhancement in the thermal conductivity of nanofluid as compared to that of oil based CNT nanofluid. The average size of the multiwalled CNTs used is 30 nm in diameter and 10–50  $\mu\text{m}$  in length. The experiments show an enhancement of 11.3% at 1% volume of the CNTs and around 4% enhancement at 0.25% volume concentration.

Although the enhancement is relatively less as compared to the CNT in oil nanofluid, still it is much higher as compared to the classical model predictions. The present model over-predicts it by a little, however, gives a reasonable idea about the order of enhancement. The liquid particle size for water used for calculations is 2  $\text{\AA}$ . The linear dependence of the thermal conductivity of CNT nanofluid on the CNT concentration is once again confirmed.

The success of the model is in predicting both, very high and very low enhancements in the thermal conductivity of CNT nanofluids. The success of the model for other types of CNT nanofluids may depend on the other factors as well such as aspect ratio or length of the CNTs, as it will play a major role in fulfilling the requirement of a continuous medium of CNTs. Also, the type of surfactant used, hydrophobic or hydrophilic nature of CNTs may play a role in terms of the surface thermal resistance.



**Figure 2.** Comparison of model predictions with concentration variation for CNT in oil nanofluid.



**Figure 3.** Comparison of model predictions with concentration variation for CNT in water nanofluid.

#### 4. Conclusions

An existing theoretical model for predicting thermal conductivity of nanoparticle suspensions is improved so as to predict the thermal conductivity of CNT nanofluids. This is a completely new approach to model the thermal conductivity of CNT nanofluids. The model predictions successfully match the experimental data, varying over two orders of magnitude in their thermal conductivity enhancement values. The model predicts linear variation of the thermal conductivity of CNT nanofluid with volume concentration, which matches with the experimental data. It also predicts direct dependence on the thermal conductivity of CNTs and inverse dependence on the thermal conductivity of base liquid. Although the model is empirical in its derivation, however, it does not use any empirical constant.

#### Nomenclature

$A_1$ , Heat transfer area per particle for conduction through liquid medium ( $m^2$ );  $A_s$ , surface area of nanoparticle ( $m^2$ );  $d_p$ , average particle diameter (m);  $k_l$ , thermal conductivity of liquid medium (W/mK);  $k_s$ , thermal conductivity of particle (W/mK);  $q$ , heat flux by conduction ( $W/m^2$ );  $T$ , temperature (K).

#### Subscripts

eff, Effective; l, liquid medium; s, solid medium.

#### Greek symbols

$\varepsilon$ , Particle volume fraction.

#### References

- Assael M J, Metaxa I N, Arvanitidis J, Christophilos D and Lioutas C 2005 *Int. J. Thermophys.* **26** 647  
 Biercuk M J, Llaguno M C, Radosavljevic M, Hyun J K, Johnson A T and Fischer J E 2002 *Appl. Phys. Lett.* **80** 2767  
 Choi S U S, Zhang Z G, Yu W, Lockwood F E and Grulke E A 2001 *Appl. Phys. Lett.* **79** 2252  
 Gao L and Zhou X F 2006 *Phys. Lett.* **A348** 355  
 Hamilton R L and Crosser O K 1962 *I&C Fundam.* **1** 187  
 Hemanth K D, Patel H E, Rajeev K V R, Sundararajan T, Pradeep T and Das S K 2004 *Phys. Rev. Lett.* **93** 144301  
 Hwang Y J, Ahn Y C, Shin H S, Lee C G, Kim G T, Park H S and Lee J K 2006 *Curr. Appl. Phys.* 1068  
 Liu M S, Lin M C C, Huang I T and Wang C C 2005 *Int. Comm. Heat Mass Transf.* **32** 1202  
 Maxwell-Garnett J C 1904 *Philos. Trans. R. Soc. London, Series A* **203** 385  
 Nan C W, Shi Z and Lin Y 2003 *Chem. Phys. Lett.* **375** 666  
 Nan C W, Liu G, Lin Y and Li M 2004 *Appl. Phys. Lett.* **85** 3549  
 Xue Q Z 2005 *Physica* **B368** 302