Film spreading from a miscible drop on a deep liquid layer

Raj Dandekar,[1] Anurag Pant[2] and Baburaj A. Puthenveettil[2]†

[1]Department of Mechanical Engineering, Indian Institute of Technology Madras, Chennai, 600036, India.

[2]Department of Applied Mechanics, Indian Institute of Technology Madras, Chennai, 600036, India.

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We study the spreading of a film from ethanol-water droplets of radii 0.9 mm$< r_d <$ 1.1 mm on the surface of a deep water layer for various concentrations of ethanol in the drop. Since the drop is lighter ($\xi = \rho_l/\rho_d > 1.03$), it stays at the surface of the water layer during the spread of the film from the drop; the film is more viscous than the underlying water layer since $\chi = \mu_l/\mu_d > 0.38$. Inertial forces are not dominant in the spreading since the Reynolds numbers based on the film thickness h_f, are in the range $0.02 < Re_f < 1.4$. The spreading is surface tension driven since the film Capillary numbers are in the range $0.0005 < Ca_f < 0.0069$ and the drop Bond numbers in the range $0.19 < Bo_d < 0.56$. We observe that when the drop is brought in contact with the water surface, capillary waves propagate from the point of contact, followed by a radially expanding, thin circular film of ethanol water- mixture. The film develops instabilities at some radius to form outward moving fingers at its periphery while it is still expanding, till the expansion stops at a larger radius. The film then retracts, during which time the remaining major part of the drop, which stays at the center of the expanding film, thins and develops holes and eventually mixes completely with water. The radii of the expanding front of the film scales as $r_f \sim t^{1/4}$ and shows dependence on the concentration of ethanol in the drop as well as on r_d, and is independent of the layer height h_l. Using a balance of surface tension and viscous forces within the film, along with a model for the fraction of the drop that forms the thin film, we obtain an expression for the dimensionless film radius $r_f^* = r_f/r_d$, in the form $f r_f^* = {t_{\mu d}^*}^{1/4}$, where $t_{\mu d}^* = t/t_{\mu d}$, with the time scale $t_{\mu d} = \mu_d r_d/\Delta\sigma$ and f is a function of Bo_d. Similarly, we show that the dimensionless velocity of film spreading, $Ca_d = u_f \mu_d/\Delta\sigma$, scales as $4f^4 Ca_d = {r_f^*}^{-3}$.

1. Introduction

A lighter, miscible drop of lower surface tension on the surface of a deep horizontal fluid layer of higher surface tension shows a fascinating interplay of surface tension driven film spreading, instability of the spreading film, followed by its retraction and the eventual dissolution of the drop. In addition to the unclear physical processes behind these phenomena, these are also important in many applications like drug delivery (Grotberg 1994), coating processes (La Due, Muller & Swangler 1996), ink-jet printing (Le 1998) and the removal of oil spills (Fay 1969). The present study presents the various phenomena that occur in such a case and then proposes a scaling theory for the spreading of a film from a buoyant, miscible drop of lower surface tension but higher viscosity on a deep layer of higher surface tension liquid of lower viscosity; the observed scaling and its proposed explanation being different from the previous studies with very viscous drops (Bacri, Debregeas & Brochard-Wyart 1996) or with soluble/insoluble surfactant drops (Halpern & Grotberg 1992; Jensen & Grotberg 1993).

When an insoluble drop comes in contact with the horizontal surface of a liquid layer, when the

† Email address for correspondence: apbraj@iitm.ac.in

surface tension of the liquid layer is larger than that of the drop ($\Delta\sigma = \sigma_l - \sigma_d > 0$), often due to the drop being a surfactant drop, an outward horizontal force acts on the drop which spreads it. The spreading is found to occur in the form of a film (Joos & Pintens 1977), the film being assumed to be a monolayer for the spreading of surfactant drops. Here, as well as in all later notations, we use the subscript f to denote the spreading film, d to denote the drop and l to denote the liquid layer beneath the film that spreads from the drop. In such a situation, the monolayer is assumed to have no viscous dissipation in it and is expected to spread as a rigid sheet (Jensen & Grotberg 1993). The increase of film radius (r_f) with time is then determined by the nature of viscous dissipation in the underlying liquid layer, which differs for thin ($\epsilon = h_l/r_d \ll 1$) and deep ($\epsilon \gg 1$) layers, where h_l is the liquid layer thickness and r_d the initial drop radius. We focus on the previous deep layer results below since the present study is for deep layers, the reader is referred to the review of Grotberg & Gaver III (1996) and the papers by Jensen & Halpern (1998) and Dussaud *et al.* (2005) for the thin layer results.

For the spreading of a low viscosity insoluble surfactant drop on a deep liquid layer, Landt & Volmer (1926); Fay (1969); Joos & Pintens (1977) and Joos & Van Hunsel (1985) proposed that the balance of the viscous resistance in a boundary layer below the spreading surfactant monolayer with the driving interfacial tension force results in the dimensionless film radius, $r_f^* = r_f(t)/r_d = (2/\sqrt{3}){t_{\mu l}^*}^{3/4}$, where $t_{\mu l}^* = t/t_{\mu l}$, with $t_{\mu l} = (\rho_l \mu_l r_d^4/\Delta\sigma^2)^{1/3}$ being the viscous-capillary time scale for deep layers, and $\Delta\sigma$ has to be replaced by the spreading parameter if the interfacial tension between the spreading and the underlying liquid is also important. The same scaling was written by Jensen (1995) as $r_f(t) \sim (A^2 M^2 t^3/\mu\sigma_d)^{1/8}$ for the mass M of the surfactant drop and $A = d\sigma/d\Gamma$, with Γ being the local surfactant concentration; the expression reduces to the $3/4^{th}$ power law when $\Gamma \sim M/r_f^2$ and $A \sim \Delta\sigma/\Gamma$. The similarity solution for the spreading of a strip of viscous oil over water also show the $3/4^{th}$ power law, when the underlying boundary layers dominate (Foda & Cox 1980). The experimental evidence for this $3/4^{th}$ power law is not conclusive. For the spreading of surfactants, the $3/4^{th}$ law has been observed for low viscosity FC-129 on CCl_4, however, not for the low viscosity CTAB/PFAC mixture on benzene, which showed an exponent of 0.575 (Joos & Van Hunsel 1985). Further, even when high viscosity silicone oil (965 cP) spreading on water obeyed this law (Dussaud & Troian 1998), 20cP PDMS on 100cP Glycerine-water solution showed $r_f \sim t^{0.4}$ while spreading of 1000cP PDMS on the same substrate showed $r_f \sim t^{0.5}$ (Fraaije & Cazabat 1989).

When the spreading drop is very viscous, Bacri *et al.* (1996), not considering the film around the drop, proposed that the dimensionless drop diameter, $r_d^* = r_d(t)/r_d \sim {t_{\mu d}^*}^{1/4}$, where, $t_{\mu d}^* = t/t_{\mu d}$, with $t_{\mu d} = \mu_d r_d/\sigma_e$ being the viscous-capillary time scale for the drop and σ_e is the effective surface tension, defined as the harmonic mean of the interfacial tensions on drop-air and drop-liquid layer interfaces. This scaling was proposed to occur when the dominant viscous dissipation inside the spreading drop balanced the surface tension force at the triple line. The $t^{1/4}$ scaling was observed by Bacri *et al.* (1996) in extremely viscous PDMS (29310 cP to 97700 cP) spreading over glycerol-water mixture (5.97 cP to 934cP) till $r_d(t)/l_c < 1$, where the capillary length $l_c = \sqrt{\sigma_e/\rho_e g}$ with $\rho_e = \rho_d(1 - \rho_d/\rho_l)$ as the effective density; the dependence of $r_d(t)$ on other fluid properties and the initial drop diameter r_d was however not verified.

If the spreading drop is also soluble in the underlying liquid layer, the geometry of spreading depends on the rate of adsorption of the drop fluid into the liquid layer, however, the spreading rate still remains largely unaffected, as was proposed by Jensen & Grotberg (1993, 1992) and experimentally verified by Afsar-Siddiqui *et al.* (2003) for very thin liquid layers. In the case of volatile, less viscous drops of various fluids, which spread on a more viscous,deep water layer, in which they are insoluble, Dussaud & Troian (1998) found that the radius of the film increases for all cases as $t^{1/2}$. The difference from the expected $3/4^{th}$ power law was hypothesised to be due

to the cooling of the film by evaporation which would change the nature of the boundary layer below the film from a Blasius type. However, other reasons also give a $t^{1/2}$ power law, as was found by Bacri *et al.* (1996) for the spreading of viscous drops when the spreading drop radius becomes larger than l_c, in which case the viscous dissipation inside the drop balances the work done by gravitational forces.

As the above discussion has shown, the spreading of drops on deep fluid layers is complex and inadequately understood, with different scaling laws being proposed in different parameter regimes. These scalings also do not seem to be fully verified since most verification experiments study only the time dependence of the spreading radius, without studying the effect of the property ratios of the drop and the substrate fluid. Another consideration that has been unexplored is the role of the initial radius of the drop on its spreading rate, through its ability to influence the initial conditions as well as through its effect on the flux of drop fluid into the spreading film. A commonly encountered regime, namely, the film spreading of a slightly more viscous liquid on a less viscous deep layer, especially when the spreading liquid is not a surfactant so that significant viscous dissipation could occur in the spreading film has not been explored. In such a case, when the drop fluid is also soluble and volatile, the scaling law for spreading is even less known. Such a regime is important as it is commonly encountered in the spreading and eventual mixing of short chain alcohols on solvents like water, which have many technological applications.

In this paper we study the film spreading from drops of ethanol-water mixture, of ethanol concentrations $20\% \leq C_e \leq 100\%$, and radii 0.9 mm$< r_d <$ 1.1 mm on the surface of a thick layer ($h_l = 5$mm) of water. The spreading occurs very fast, and is over within about 0.5s since it is surface tension driven, as shown by the range of the film Capillary numbers, $Ca_f = \mu_f u_f/\Delta\sigma$, $0.0005 < Ca_f < 0.0069$. However, since the film Reynolds numbers ($Re_f = u_f h_f/\nu_f$) are in the range of $0.02 < Re_f < 1.4$, viscous forces are more than inertial effects. Further, due to high surface tension forces, the film Weber numbers are also small ($We_f = \rho_f u_f^2 h_f/\Delta\sigma < 0.005$); inertia in film spreading dynamics is negligible. The drop is also lighter than the underlying liquid with the range of density ratios ($\xi = \rho_l/\rho_d$) being $1.27 > \xi > 1.03$ so that it stays at the free surface while the film spreads; the drop remains an approximate ellipsoid form since the range of drop Bond numbers ($Bo_d = \rho_d g r_d^2/\Delta\sigma$) was $0.19 < Bo_d < 0.56$. Surface tension dominates over gravitational forces in the spreading process since the Bond number based on film thickness will be even smaller. Eventhough the drop is more viscous than the underlying layer, with the range of viscosity ratios ($\chi = \mu_l/\mu_d$) being $0.81 > \chi > 0.4$, since the film Ohnersorge number $Oh_f = \mu_f/\sqrt{\Delta\sigma\rho_f h_f} \sim 10^{-2}$, surface tension dominate over viscous resistance in spreading In such a situation, we show that, different from the earlier suggested regimes of film spreading, a balance of viscous resistance in the film with the driving surface tension force gives rise to a $r_f \sim t^{1/4}$ scaling law. More importantly, by modelling the initial coalescence of the drop with the liquid layer, we estimate the initial fraction of the drop that forms the film. By including this fraction in the scaling analysis, we clarify the dependence of the spreading rate on the initial drop radius and the property ratios of the drop and the liquid layer. The paper is organised as follows. we describe the experimental setup and procedure in § 2 followed by a qualitative description of the spreading phenomena in § 3. The proposed scaling law is developed and verified in detail in § 4 before concluding the paper by discussing the implications of the proposed scaling in § 5.

2. Experiments

The experiments were conducted by adding ethanol-water drops of varying concentrations of ethanol(C_e) and radii (r_d) to the surface of a water layer of height $h_l = 5$mm in a petri dish of 100mm diameter, as shown in the schematic of figure 1. Larger height experiments with $h_l = 75$mm were also conducted in a 85mm diameter beaker. The drops were produced from

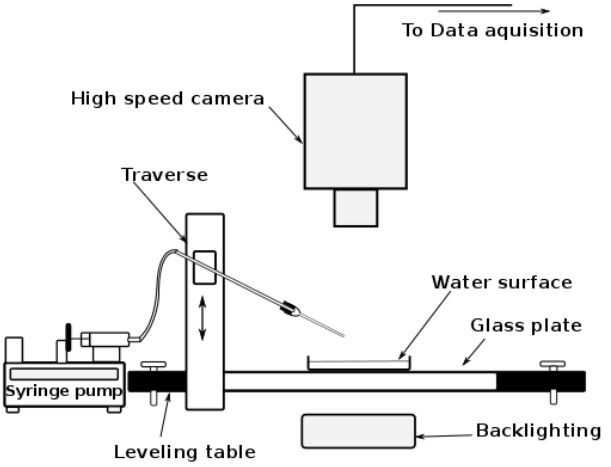


FIGURE 1. Schematic of the experimental set up.

C_e	σ_d	μ_d	$\Delta\sigma$	ρ_d	r_d	h_f	Bo_d	Oh_f	Re_f	We_f	Ca_f
(%)	(mNm^{-1})	(cP)	(mNm^{-1})	(kg/m^3)	(mm)	(μm)		(10^{-2})		(10^{-3})	(10^{-4})
20	37.97	1.76	16.03	970.36	0.97	8.4-14.7	0.56	11.6-15.3	0.1-0.42	0.3-2.4	26-57
40	31	2.34	23	948.47	0.97	13.4-18.4	0.38	11.7-13.6	0.22-0.49	0.9-3.4	41-69
60	26	2.24	28	908.72	0.97	5.9-11.7	0.3	13-18	0.03-0.22	0.04-0.85	12-38
80	23.8	1.66	30.2	859.58	0.97	3.3-10.4	0.26	10-17	0.02-0.19	0.01-0.39	7-20
100	22	1.1	32	790.74	0.97	3.3-8.8	0.22	4.9-9.9	0.06-1.4	0-5	6-35
100	22	1.1	32	790.74	0.9	3.5-8.3	0.19	7.6-11.8	0.04-0.23	0.03-0.32	6-14
100	22	1.1	32	790.74	1.1	4.8-9	0.29	7.3-10	0.05-0.21	0.03-0.24	5-11

TABLE 1. Properties of the drop, the driving surface tension difference, the drop Bond number and the range of relevant dimensionless numbers of the film. The properties of the drop at different concentrations are at 25°C, obtained from Ernst *et al.* (1936); Blanchette *et al.* (2009) and Khattab *et al.* (2012). The properties of the underlying water layer are $\sigma_l = 54$mNm^{-1}, $\mu_l = 0.89$cP and $\rho_l = 1000$ kg/m^3.

capillaries of different sizes connected to a syringe pump. The flow rate of the syringe pump was fixed low (2.4ml/hr) so that the liquid coming out from the capillary was in the dripping regime (Clanet & Lasheras 1999). The equivalent spherical radius of the drop (r_d) was determined from the number of drops required to fill a specific volume for each of the capillaries used; the values of r_d are shown in Table 1. Care was taken to maintain the flow rate and the orientation of the capillary to be the same in all experiments with each capillary. The height of the capillary tip was adjusted so that the drops detached from the capillary very close to the free surface to avoid inertial effects due to the impingement of the drop on the water surface. The range of concentrations of the ethanol-water drops, the corresponding densities (ρ_d), surface tension with air (σ_d), and kinematic viscosities (μ_d) of the drop solutions are shown in Table 1.

The topview visualizations of the spreading dynamics, shown in figure 2, was done using Aluminium particles, which when mixed with water, forms a thin layer of particles at the free surface. As determined by a particle size analyser (Microtrac Inc), the aluminum particles had a median diameter of 14.65μm, mean diameter of 5.09μm, with the particle diameters distributed in an asymmetric distribution between 0.3μm and 100μm. At the concentration of the particles used (163 ppm), the surface tension of water was measured as 54mNm^{-1}, the details of which are given in Appendix A. The top view of the spreading dynamics was captured by a high speed

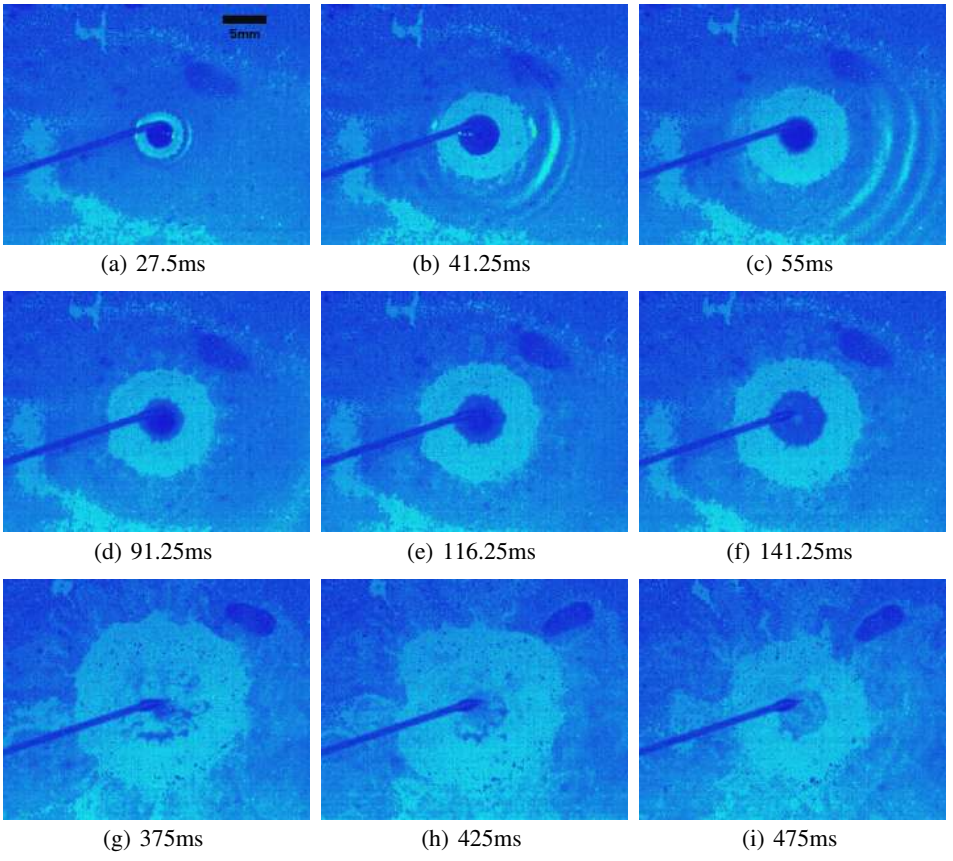
camera (LaVision ProHS) at about 800fps with LED backlighting as shown in figure 1. In some cases, 5ppm of Rhodamine 5B was added to the drop in these top view visualisations so as to distinguish the drop fluid from the underlying water layer. The surface tension reduction at 5ppm dye concentration was measured to be 0.14%, which is negligible to affect the dynamics. The spreading radius of the film $r_f(t)$ was measured as the radius of the circular region devoid of tracer particles, as seen in figure 2(c), from such top view images at increasing times t, the time calculated from the frame number of the image, knowing the FPS. The center of measurement was fixed as the tip of the capillary seen in top view images and zero time as the time of contact of the drop with the liquid surface. The film radius in each image was calculated as the mean from three measurements, taken at three azimuthal locations on the film where a minimum local radius of the film could be identified; the locations spanned the full circumference of the film. The velocities of expansion of the film front u_f were calculated by taking the time derivative of the power law fit through the increasing part of r_f vs t. A sample fit for $C_e = 60\%$ and $r_d = 0.97$mm is shown in the inset of figure 4. The errors associated with the measurement of r_f, t and u_f are discussed in Appendix B. In addition, to understand the coalescence of the drop with the water layer and the subsequent spreading of the film, high speed shadowgraphy visualisations of the side view were conducted in a 5cm $\times$ 5cm cross section glass tank with $h_l = 5$cm, using a Photron SA5 camera at 2000 FPS. Hollow glass spheres of 10 μm diameter were added in the water layer and backlighting was used to obtain shadowgraphy combined with particle visualisation; a typical image sequence obtained is shown in figure 3. Images with large exposure time, of laser induced fluorescence of 6μm fluorescent particles in the drop and scattering from 10μm hollow glass spheres in water by a vertical laser sheet was used to observe vortices, as shown in figure 3(i).

3. Description of the phenomena

3.1. *Coalescence and spreading dynamics*

Figure 2 shows the top views of the sequence of spreading of an ethanol drop of $C_e = 100\%$ and $r_d = 0.97$ mm. The local depression in surface tension caused at the point of contact of the drop with water results in radially outward Marangoni forces which cause a thin film of ethanol-water mixture to spread. The expanding white circular region that is free of particles, seen in figures 2(a) - 2(c), shows the spreading film. We also notice the initiation and propagation of capillary waves ahead of the expanding film in figures 2(a) to 2(c). After some time(90 ms), the outer front of the film develops instabilities resulting in outward moving fingers or plumes as seen in figures 2(d)-2(f). Eventhough there is an inward flow in between these outward growing fingers, the radius of the continuous film region, as well as the circular region covering the outer tips of the growing fingers go on increasing in time, however, with decreasing velocities (see movie 1 online). The length of the fingers increase along with the radius of the continuous film region, until the velocity of expansion of the continuous film reduces to zero, after which the continuous film region begins to retract inwards (figures 2(g) -2(i)) while the outer tips of the fingers remain approximately stationery in time. The total time of film expansion is about 0.4s. Most of the drop remains at the center of the expanding film during the whole time of film expansion, seen as the dark circular region at the centre of the expanding film in figures 2(a) -2(f). This remnant part of the drop also expands, however at a much slower rate than the film, thins and then develops holes in it. The remnant drop eventually gets mixed with water by a combination of convection and diffusion, after the continuous film has started retracting, as seen in figures 2(g) -2(i); the total time from contact to dissolution being about 0.6s.

The side views of the film spreading process for a similar concentration drop with $r_d = 1.1$ mm, shown in figure 3, clarifies the critical role of the initial coalescence between the drop and the water layer in film formation. Regions marked as A in figures 3(a) to 3(f) show that a small



(a) 27.5ms (b) 41.25ms (c) 55ms

(d) 91.25ms (e) 116.25ms (f) 141.25ms

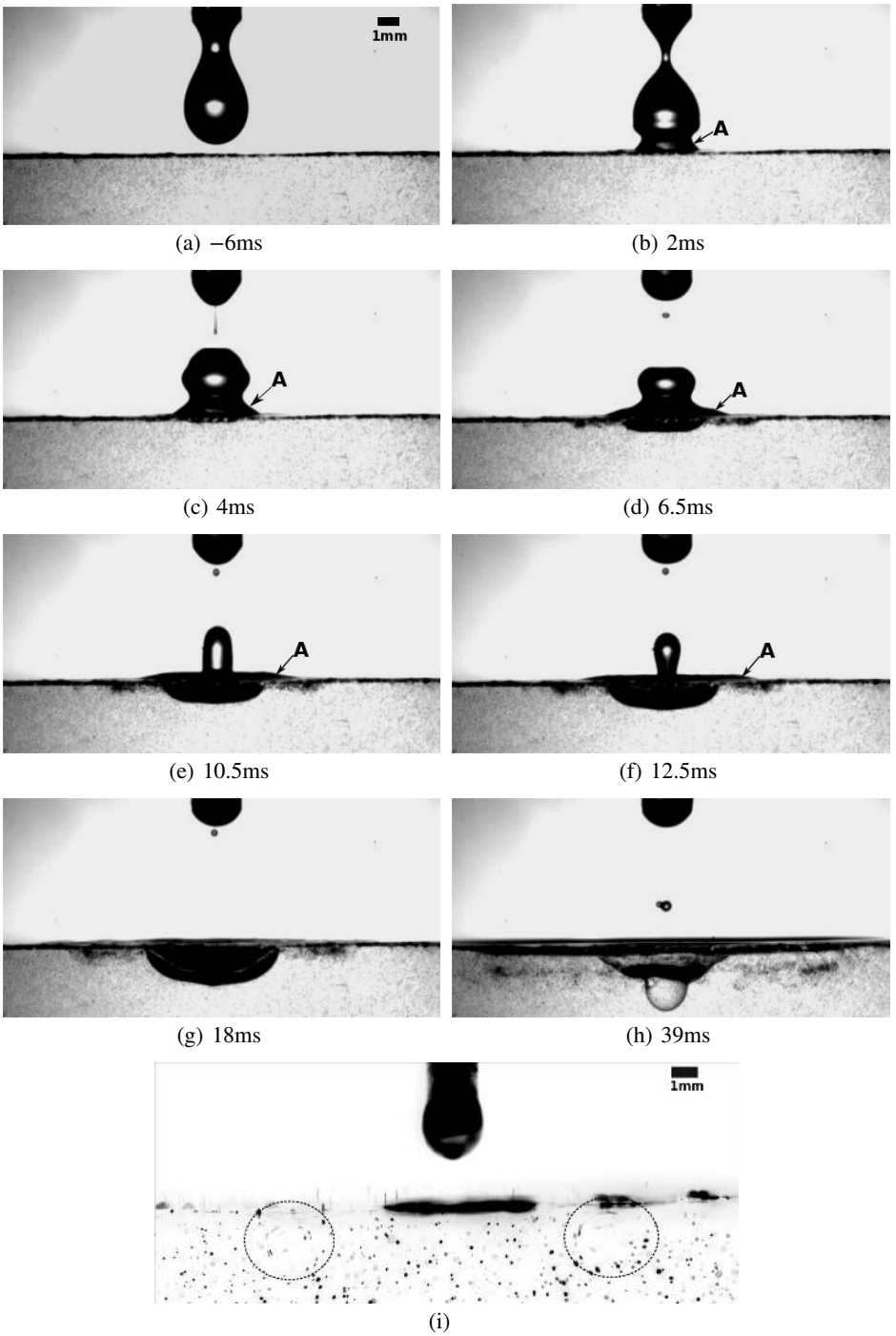
(g) 375ms (h) 425ms (i) 475ms

FIGURE 2. Top views of the sequence of spreading and eventual mixing of a 100% ethanol drop of radius $r_d = 0.97$mm on the surface of a water layer of height $h_l = 5$mm. 2(a)-2(c): capillary wave propagation followed by the expanding circular film, seen as the white circular region. The dark circular region at the centre of the expanding film is the drop, dyed with Rhodamine 5B. 2(d)-2(f): expanding film becomes unstable at its outer periphery and then develops outward propagating fingers. 2(g)-2(i): drop at the centre of the film develops holes and eventually mixes, while the film retracts. The size of each image is 35mm × 22.5mm. See movie 1 online.

fraction of the drop, from its bottom, gets pulled apart by the neck expansion during coalescence and becomes the source of the drop fluid in the film (see movie 2 online). As these figures show, the major part of the drops goes down and then bounces back due to its buoyancy, while the initial bottom part of the drop gets pulled apart to form the spreading film. It could also be noticed that there is no substantial motion in the regions below the spreading film, except for a vertical redistribution of the particles at the interface seen as the dark region below the film in figures 3(g) and 3(h). Such a distribution of particles at the interface occurs because of the vertical momentum imparted to the interface due to the vertical oscillations of the drop due to the ligament retraction dynamics during pinch off from the capillary. We now look at the quantitative variation of the radius of the expanding continuous circular film (r_f) as a function of time (t), measured as discussed in § 2, from images similar to that in figure 2.

3.2. *Spreading radius and velocity*

Figure 4 shows the measured values of $r_f(t)$ as a function of time t for different C_e (hollow symbols), with different r_d (solid symbols) and with different h_l(hollow symbol with dot), the



(a) −6ms (b) 2ms

(c) 4ms (d) 6.5ms

(e) 10.5ms (f) 12.5ms

(g) 18ms (h) 39ms

(i)

FIGURE 3. (a) to (h): Side views of the sequence of coalescence and film spreading when an ethanol drop of radius $r_d = 1.1$mm and 100% concentration mixes with a water layer of $h_l = 5$cm height. The point A shows the fraction of the drop being drawn apart by coalescence that forms the spreading film. The size of each image is 16.88mm × 8.4mm. (i) Side view visualisation of film spreading from a drop of $r_d = 1.1$mm and $C_e = 100\%$ with 10μm hollow glass spheres in the substrate and 6μm fluorescent particles in the drop. The dashed circles show the tip vortices at the periphery of the spreading film. The image shown is the negative of the obtained image for clarity and is of size 22.5mm × 9.08 mm. See movie 2 online.

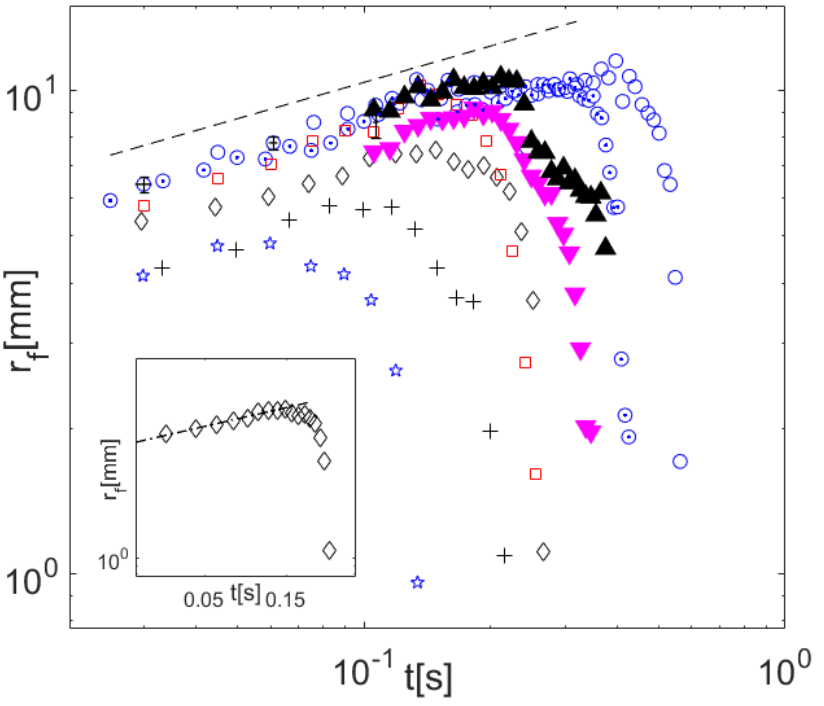


FIGURE 4. Variation of the film radius with time for different drop radii, ethanol concentrations and layer height. The hollow symbols represent $r_d = 0.97$mm with varying ethanol concentrations in the drop, ○, C_e=100%; □, C_e=80%; ◇, C_e=60%; ☆, C_e=40%; +, C_e=20%. The solid symbols represent experiments with 100% concentration with varying r_d, ▼, r_d=0.9mm; ▲, r_d=1.1mm. The experiments with hollow and solid symbols had the water layer height $h_l = 5$mm. An experiment with a larger layer height $h_l = 75$mm, C_e=100% and $r_d = 0.97$ mm is shown by ⊙. The dashed line shows the 1/4 slope of the data. The inset shows the r_f vs t data for $C_e = 60\%$ and $r_d = 0.97$ mm along with the curve fit $r_f = 11.89t^{0.232}$, from which the velocity is calculated.

zero time being at the instant of contact of the drop with water. The horizontal error bars in the figure shows the error in time measurement due to the uncertainty of the time of contact, discussed in Appendix B. As discussed in Appendix B, r_f is the mean of three azimuthal measurements; the range of these three measured radii is shown in figure 4 for $C_e = 100\%$ and $r_d = 0.97$mm as the vertical bars. This range increases in the later measurements since the film develops azimuthal instabilities after expanding for some time to forms fingers in its outer periphery, as we saw in figure 2(d). After this instability occurs, $r_f(t)$ is measured as the radius of the continuous film, not including the region with fingers. The plot includes measurements after the instability at the edge of the film occurs; no change in the rate of expansion of r_f is seen after the instability occurs.

The radius, r_f increases as the continuous film region expands with time (figure 2(a) to 2(g)) and then starts to decrease with time once the film front starts to retract (figure 2(g) to 2(i)). The inset in the figure shows the curve fit that is used to calculate the film expansion velocity (u_f) for one experiment, as discussed in § 2. The film expansion velocities(u_f) decrease with time, as shown in figure 5. The initial ($t \approx 0.03$s) expansion velocities of the film are high (> 10 cm s^{-1}), which reduces to zero beyond which the velocities reverse their direction due to film retraction. Retraction occurs over a shorter time than expansion, for example, for $r_d = 0.97$ mm and C_e= 100%, shown with ○ in figure 4, film expansion occurs over 0.4 s while retraction occurs over 0.2 s.

Figure 4 shows that at any time, a larger C_e in the drop results in a larger radius of the film.

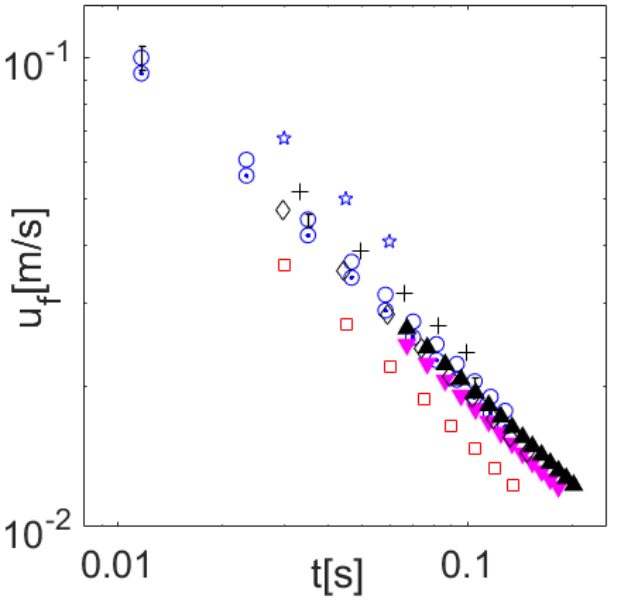


FIGURE 5. Variation of the film expansion velocity with time for different drop radii, ethanol concentrations and layer height. The symbols are the same as in figure 4.

The slope of r_f vs t for different ethanol concentrations are approximately the same, indicating the same power law dependence of r_f on t for different ethanol concentrations; this power law is approximately $t^{1/4}$ as shown by the dashed line in figure 4. For the same r_d, higher the concentration of ethanol in the drop, larger is the maximum r_f and larger is the time of spreading. It could also be noticed that at any specific time, r_f has a non monotonic dependence on the initial radius of the drop r_d. The hollow circles and the hollow circles with a center dot in figure 4 are identical experiments except that the water layer height (h_l) was 15 times larger in the latter. These two data sets fall on each other implying that the radius r_f at any time, the exponent of the power law of r_f vs t, as well as the velocity of spreading are all independent of the height of the underlying liquid layer; this independence of h_l paves way to our scaling analysis in § 4 . We now proceed to find scaling relations for these dependences of r_f on time, r_d and the fluid properties. The scaling analysis presented in this paper is limited to the expanding radius of the spreading film, and does not include the retraction of the film.

4. Scaling Analysis

As we saw in § 3.2, the spreading radius r_f and velocities u_f are independent of h_l, the underlying liquid layer height. Such would be the case if viscous dissipation in a boundary layer below the film was the dominant resistance for the spreading film, as discussed in § 1; this would however give $r_f \sim t^{3/4}$, quite different from the observed time dependence in figure 4. The ratio of viscous stress due to a Blasius boundary layer below the spreading film $\tau_{bl} = \mu_l u_f/\delta_{bl}$ to the viscous stress in the film $\tau_f = \mu_f u_f/h_f$ is,

$$\frac{\tau_f}{\tau_{bl}} = \frac{\mu_f}{\mu_l}\frac{\delta_{bl}}{h_f}, \tag{4.1}$$

where δ_{bl} is the Blasius boundary layer thickness. When $t = 0.2$s and $r_f = 10$mm at the end of the expansion of the film for $C_e = 100\%$ and $r_d = 0.97$mm, we have $\delta_{bl} \sim \sqrt{\nu_l t} \approx 400\mu$m and

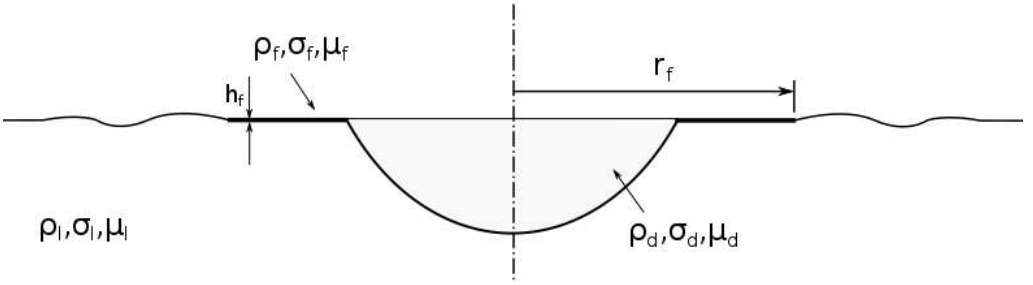


FIGURE 6. Schematic of film spreading from a lighter miscible drop on a deep liquid layer showing the symbols used.

$h_f = 4r_d^3 G/3r_f^2 \approx 5.33\mu$m (see (4.2) and (4.21 later), resulting in $\tau_f/\tau_{bl} \approx 75$. The film viscous stress is about two orders of magnitude higher than the stress due to a possible Blasius boundary layer in the present case. Similarly, the viscous extensional stress in the film, $\tau_e \sim \mu_f u_f/r_f$. The ratio $\tau_f/\tau_e \sim r_f/h_f \sim 1876$, using the above values of r_f and h_f; the viscous shear stress in the film is hence three orders of magnitude higher than the viscous extensional stress in the film.

We hence consider the situation where the spreading dynamics is likely to be determined by the balance of viscous shear stresses within the film with the driving surface tension force; a similar assumption has been made by (Hernández-Sánchez, Eddi & Snoeijer 2015) for spreading due to a continuous supply of IPA. We also saw in § 3.1 that during the period of spreading of the film, only a fraction of the volume of the drop is pulled apart by the neck expansion which then spreads as the film. Based on these observations and on the assumption that the initial fraction of the drop mass remains well mixed while spreading as the film, we now develop a scaling analysis below. The analysis uses the balance of forces within the spreading film and an estimate of the initial fraction obtained from coalescence dynamics. The resultant scaling law captures the dependence of r_f and u_f on time, the initial radius of the drop and on the initial concentration of ethanol in the drop, which as we saw in § 3.2 are the prime variables on which the spreading depends on.

4.1. *Mass and momentum balance*

We assume the spreading to be as shown in the figure 6. As we saw in § 3.2, the film spreading is rapid, with the spreading being over in 0.4 s for the 100% ethanol drop. Further, as could be seen from figure 2, only a small fraction of the drop spreads as the film during the time of film spreading. Due to the small characteristic time of spreading ($t_{\mu f} \sim r_f/u_f$), we assume that the film is well mixed during its spreading so that the density of the film remains a constant over the short time of spreading. This assumption implies that the loss of ethanol from the film during spreading due to evaporation and mixing with the underlying water layer is small. As shown in Appendix C, the evaporation velocities are of the order of 10^{-5}ms^{-1} while $u_f \sim 5 \times 10^{-2}$ms^{-1}; evaporative flux in $t_{\mu f}$ will be negligible compared to the longitudinal flux in the film. Since convective mixing is absent (see figure 3), the downward mixing velocities, of the order of diffusive velocities $D/h_f \sim 10^{-4}$ms^{-1} is also negligible in time $t_{\mu f}$. When G fraction of the volume of the drop spreads as a film of constant density ρ_f, with a time dependent film height $h_f(t)$, mass balance of the drop and film implies,

$$G\frac{4}{3}\pi r_d^3 \rho_d = \pi r_f^2 h_f \rho_f, \tag{4.2}$$

Change in the radius of the drop fluid reservoir, seen as the dark centre region in figures 2(a) to 2(f) is small while the film spreads. Further, the value of $t_{\mu f}$ is small. Due to these reasons, we assume the change in volume of the drop during $t_{\mu f}$ to be negligible; the change in density of the drop is also then negligible in $t_{\mu f}$; ($d\rho_d/dt \approx 0$ when $t < t_{\mu f}$). Since mass and momentum

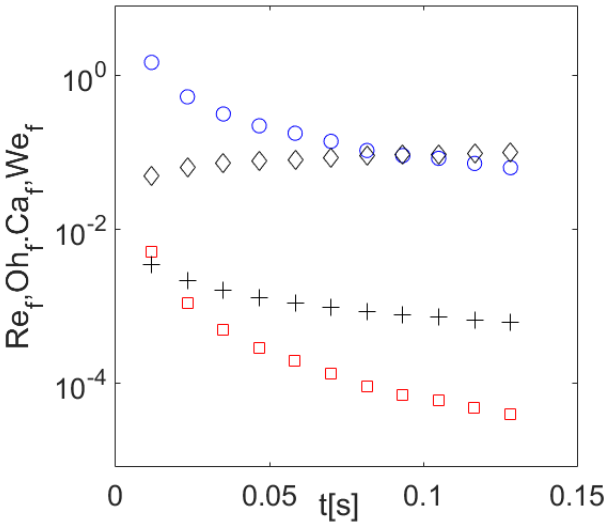


FIGURE 7. Variation of the dimensionless numbers of the film with time for an experiment with $C_e = 100\%$ and $r_d = 0.97$mm. ○, Re_f; □, We_f; ◇, Oh_f; +, Ca_f.

change of the drop reservoir over $t_{\mu f}$ are then negligible, as shown in Appendix D, the mass balance of the drop and the film reduces to,

$$2\pi r_f u_f h_f \rho_f + \pi r_f^2 \rho_f \frac{dh_f}{dt} = 0. \tag{4.3}$$

Similarly, as shown in Appendix D, using (4.3) in the momentum balance for the drop and the film and neglecting terms involving change in mass and momentum of the drop reservoir implies,

$$2\pi r_f(\sigma_l - \sigma_f) - \mu_f \frac{u_f}{h_f}\pi r_f^2 = \pi r_f^2 h_f \rho_f \frac{du_f}{dt}. \tag{4.4}$$

4.2. *Scaling of spreading radius and velocity*

We now estimate the range of dimensionless numbers of the film during its spreading so as to simplify (4.4). We assume that the spreading occurs fast enough to neglect the mixing of the film with the underlying water layer, so that the film properties are the same as the drop properties, implying, $\rho_f = \rho_d$, $\sigma_f = \sigma_d$, and $\mu_f = \mu_d$. Figure 7 shows the variation of the dimensionless numbers of the film as a function of time in a typical experiment of 100% ethanol drop of $r_d = 0.97$mm. The Weber numbers based on film thickness ($We_f = \rho_f u_f^2 h_f/\Delta\sigma$) are much less than one ($0 < We_f < 0.005$) implying that the surface tension effects are much more than the inertia effects in film spreading. Similarly, since the Reynolds numbers based on film thickness ($Re_f = \rho_f u_f h_f/\mu_f$) are in the range $0.06 < Re_f < 1.4$, viscous effects are more than inertia effects, except at the beginning of the film spreading when Re_f is of order one. The Capillary numbers ($Ca_f = \mu_f u_f/\Delta\sigma$) are very small ($0.0006 < Ca_f < 0.0035$); surface tension forces dominate over viscous resistance. The values of Ohnersorge numbers ($Oh_f = \mu_f/\sqrt{\rho_f h_f \Delta\sigma}$) are in the range of $0.049 < Oh_f < 0.099$; surface tension is predominant than viscous effects.

Based on the order of these dimensionless numbers, the momentum equation (4.4) could be simplified, as follows. Since $du_f/dt \sim u_f/t_{\mu f}$ with $t_{\mu f} \sim r_f/u_f$, the ratio of the term on the RHS of (4.4) with the first term on the LHS is We_f; as seen in figure 7, $We_f \ll 1$. Similarly, the ratio of the term on the RHS of (4.4) and the second term on the LHS of (4.4) is $Re_f\left(h_f/r_f\right)$. Since $Re_f < 1$ as shown in figure 7 and $\left(h_f/r_f\right) \ll 1$ since film thickness is much smaller than

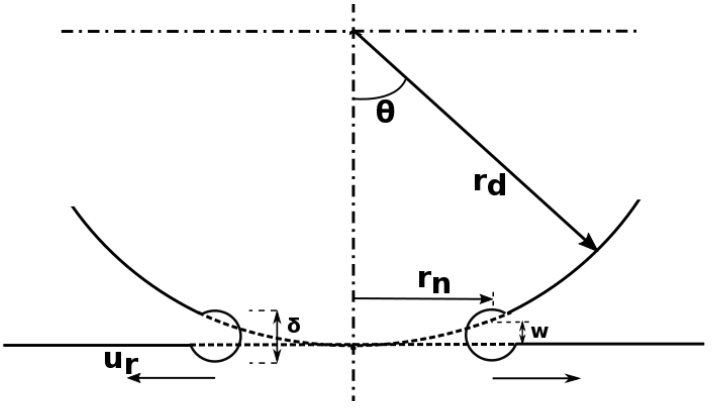


FIGURE 8. Schematic of the initial stages of coalescence of a drop with a liquid layer.

its radius; $Re_f\left(h_f/r_f\right) \ll 1$. At the same time, the ratio of the terms on the LHS of (4.4) is $h_f/Ca_f r_f$ which is of order 1, since $Ca_f \ll 1$ (figure 7) and $h_f/r_f \ll 1$. Hence, to leading order, the term on the RHS of (4.4) can be neglected. Further, assuming the film properties are the same as the drop properties, the momentum balance reduces to

$$2\pi r_f \Delta\sigma = \mu_d \frac{u_f}{h_f}\pi r_f^2. \tag{4.5}$$

Eliminating h_f from (4.2) and (4.5),

$$r_f^3 \dot{r_f} = \frac{8}{3} G r_d^3 \frac{\Delta\sigma}{\mu_d} \tag{4.6}$$

On integrating (4.6), we get

$$r_f^* = c_1 (G t_{\mu d}^*)^{1/4} \tag{4.7}$$

as the scaling of the dimensionless film radius $r_f^* = r_f/r_d$ on the dimensionless time $t_{\mu d}^* = t/t_{\mu d}$, with the characteristic time of spreading,

$$t_{\mu d} = \frac{\mu_d r_d}{\Delta\sigma}, \tag{4.8}$$

and the constant of integration $c_1 = (32/3)^{1/4}$. Since, $\dot{r_f}$=u_f, the radial velocity of film spreading, (4.6) can also be rewritten in dimensionless form as,

$$Ca_d = c_2 G {r_f^*}^{-3}, \tag{4.9}$$

where the Capillary number $Ca_d = u_f \mu_d/\Delta\sigma$ is the dimensionless spreading velocity and $c_2 = 8/3$. In the scaling laws (4.7) and (4.9), G the initial fraction of the drop that mixes to form the film is still unknown. We now obtain an expression for G based on the coalescence dynamics of the drop and the liquid layer.

4.3. *Estimation of the initial spreading fraction G*

Figure 8 shows the schematic of the initial stage of coalescence of the drop with the liquid layer, which is a schematic of the zoomed view close to the interface in figure 3(b). The fraction of the volume of the drop G that is pulled apart by the neck expansion in the coalescence time t_{co} is

$$G = \frac{2\pi r_n \delta u_r t_{co}}{\frac{4}{3}\pi {r_d}^3}, \tag{4.10}$$

where, as shown in figure 8, δ is the thickness of the neck region, r_n is the neck radius and u_r is the neck retraction velocity.

The coalescence time t_{co} in 4.10 depends on the Bond number of the drop $Bo_d = \rho_d g r_d^2/\Delta\sigma$. For low Bo_d the coalescence is purely capillary driven with the t_{co} equal to the capillary time scale $t_c = \sqrt{\rho_d r_d^3/\Delta\sigma}$, while for large Bo_d, t_{co} is equal to the gravity time scale $t_g = \sqrt{r_d/g}$ (Chen *et al.* (2006)). As shown in table 1, the range of values of Bo_d for the present experiments are $0.12 < Bo_d < 0.26$; the present experiments fall in an intermediate Bo_d range. Chen *et al.* (2006) have shown that for such a capillary-gravity regime of drop coalescence,

$$t_{co} = 0.77\sqrt{\frac{\rho_d r_d^3}{\Delta\sigma(1 + Bo_d)}}, \tag{4.11}$$

which tends to t_c as $Bo_d \to 0$ and to t_g as Bo_d becomes large.

The thickness of the neck δ in (4.10) can be estimated in the following way. From geometry of figure 8,

$$w = r_d(1 - \cos\theta), \tag{4.12}$$

which, on substitution of $\cos\theta \approx 1 - \theta^2/2$ for small θ, becomes equal to

$$w = \frac{r_d\theta^2}{2}. \tag{4.13}$$

Since $\theta \approx r_n/r_d$ for small θ from figure 8, (4.13) becomes,

$$w = \frac{r_n^2}{2r_d}. \tag{4.14}$$

Mass balance of the retracting rim resulting in a bulge of diameter δ at the tip of the rim would imply,

$$\int_0^{r_n} 2\pi r_n w dr_n = \pi\left(\frac{\delta}{2}\right)^2 2\pi r_n. \tag{4.15}$$

Evaluating the integral in (4.15), after substituting for w from (4.14), and simplifying, we get

$$\delta = \sqrt{\frac{r_n^3}{2\pi r_d}}. \tag{4.16}$$

From scaling arguments, Eggers *et al.* (1999) obtained the same relation, without the prefactor, for drop coalescence.

The neck retraction velocity u_r in (4.10) is a resultant of the balance of inertia $\rho_d u_r^2/2$ and surface tension force $\Delta\sigma/r_n$ to give

$$u_r = c_3\sqrt{\frac{2\Delta\sigma}{\rho_d r_n}}, \tag{4.17}$$

where c_3 is constant prefactor, whose value is chosen later to obtain the limiting value of G as $Bo_d \to 0$. Substituting (4.11), (4.16) and (4.17) in (4.10) and noting that $r_n/r_d \approx \theta$ for small θ in figure 8, we get

$$G \approx c_4\sqrt{\frac{\theta^4}{1 + Bo_d}}, \tag{4.18}$$

where $c_4 = 0.65c_3$. To eliminate θ from (4.18), we need one more relation of G in terms of θ,

which can be obtained as follows. From geometry of figure 8,

$$G \approx \frac{1}{2}\pi\delta r_n^2 / \frac{4}{3}\pi r_d^3. \tag{4.19}$$

Replacing δ in (4.19) from (4.16) and noting that $r_n/r_d \approx \theta$ for small θ, we get

$$G \approx \frac{3}{20}\theta^{7/2}. \tag{4.20}$$

Replacing θ in (4.18) interms of G from (4.20) results in

$$G \approx \frac{1}{2(1+Bo_d)^{7/6}}, \tag{4.21}$$

where we have chosen the prefactor $c_3 = 0.39$ so as to get $G = 0.5$ when $Bo_d \to 0$, as found by Chen, Mandre & Feng (2006).

4.4. Bo_d dependence and validation

The scaling of the dimensionless film radius (4.7) and the dimensionless film velocity (4.9) can now be expressed in terms of the drop Bond number (Bo_d) by writing G in these equations in terms of Bo_d using (4.21). By doing such a substitution, we obtain,

$$f\, r_f^* = {t_{\mu d}^*}^{1/4}, \tag{4.22}$$

and

$$4f^4\, Ca_d = {r_f^*}^{-3}, \tag{4.23}$$

where the function

$$f(Bo_d) = \frac{3^{1/4}}{2}\left(1+Bo_d\right)^{7/24}. \tag{4.24}$$

Since r_f^* in (4.23) is given by (4.22), (4.23) can also be rewritten in terms of $t_{\mu d}^*$, so as to obtain a decreasing dependence of dimensionless film velocity on time in the form $4fCa_d = {t_{\mu d}^*}^{-3/4}$. Equations (4.22) and (4.23) are the proposed scalings which are expected to capture the dependence of spreading radii and velocities on time, property ratios between the drop and the liquid layer, and the initial drop radius; we now verify these relations with our experimental data shown in figure 4.

Figure 9 shows the variation of the dimensionless spreading radius r_f^*, scaled by the function f, with the dimensionless time $t_{\mu d}^*$, plotted using the data shown in figure 4 for different C_e, r_d and h_l. The part of the data that show an increasing film radius collapse fairly well on to

$$f\, r_f^* = 0.83\, {t_{\mu d}^*}^{1/4}, \tag{4.25}$$

shown by the dashed line in the figure, the prefactor being close to the expected value of one from (4.22). The variation of the dimensionless film expansion velocity Ca_d, scaled by $4f^4$, with the dimensionless spreading radius r_f^* is shown in figure 10. Similar to that in figure 9, the data collapse fairly well on to

$$4f^4\, Ca_d = 0.5\, {r_f^*}^{-3}. \tag{4.26}$$

The data show a -3 power law exponent except for a slight deviation at small r_f^*. This deviation is expected to be due to the non-negligible inertial effects in film spreading for small r_f when the film spreads very fast (see figure 5) so that We_f becomes close to one, as seen in figure 7. The present analysis neglected the inertial effects in film spreading and is only valid when $We_f < 1$. Further, the present analysis assumed that $r_d \ll r_f$; this assumption also breaks down at small r_f when the film radius is of the size as the drop radius. The reason for the prefactors in (4.25) and

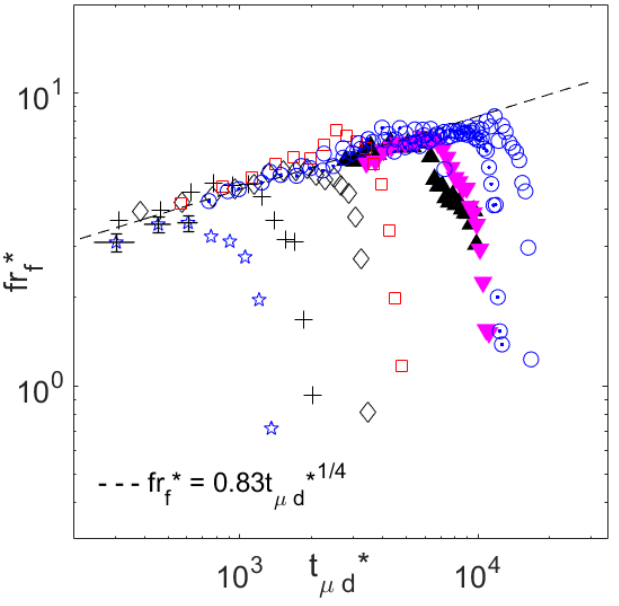


FIGURE 9. Variation of the dimensionless film radius with the dimensionless time. The symbols are as in figure 4.

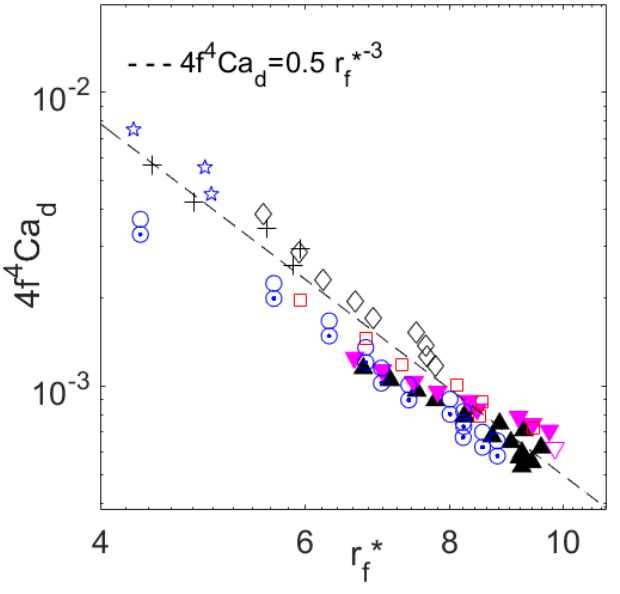


FIGURE 10. Variation of the dimensionless film velocity with dimensionless film radius. The symbols are as in figure 4.

(4.26) to be slightly less than one could be the slight inaccuracy of the prefactors assumed in the scaling relationships used in the derivation of (4.22) and (4.23).

5. Conclusions and Discussion

The primary result of this paper is the scaling law developed for the spreading radius r_f of a film, spreading from a buoyant, miscible drop, when the viscous dissipation in the spreading film is the dominant resistance to surface tension driven spreading. The proposed scaling law is,

$$r_f \sim \left(\frac{t\Delta\sigma}{\mu_d} r_d^3\right)^{1/4} \frac{1}{f}, \tag{5.1}$$

a function of two length scales $t\Delta\sigma/\mu_d$ and the initial drop radius r_d modified by a dimensionless function $f(Bo_d)$, given by (4.24). The above scaling has the correct $t^{1/4}$ time dependence shown by experiments in figure 4. The scaling law (5.1) also captures the dependence of r_f on drop properties as well as that on r_d since it collapses all the data with different ethanol concentrations in the drop(C_e) and r_d onto a single dimensionless curve $f\, r_f^* = 0.83\, {t_{\mu d}^*}^{1/4}$ (4.25), where the dimensionless time $t_{\mu d}^* = t/t_{\mu d}$ with the characteristic time of spreading $t_{\mu d} = \mu_d r_d/\Delta\sigma$, and the dimensionless film radius $r_f^* = r_f/r_d$.

The dependence of r_f on drop properties and r_d is complex since f is a function of the drop Bond number Bo_d; however the effects of property variations on r_f could be qualitatively understood by examining (5.1) and (4.24). As was shown in figure 4, r_f increases at any time t with increasing concentration of ethanol in the drop. Such an increase is captured by the positive power law dependence of r_f on $\Delta\sigma$ in (5.1); increase in $\Delta\sigma$ increases the spreading force resulting in larger r_f at any time. Increasing the concentration of ethanol in the drop shows a non-monotonic variation in the viscosity of the drop with μ_d increasing till 40% concentration and then decreasing with further increase of concentration (see table 1). A decrease in the viscosity of the drop μ_d, and hence that of the spreading film, should speed up the spreading since μ_d appears with a negative power in (5.1); such an outcome is expected due to the reduced viscous dissipation in the film with reduced μ_d. The novelty of (5.1) is that by explicitly considering the coalescence dynamics, the dependence of r_f on r_d was included in the scaling law. This dependence of r_f on r_d is non-monotonic, as seen in figure 4. The scaling (5.1) captures this non-monotonic variation since the functional dependence of r_f on r_d shown by (5.1) is non-monotonic, thereby bringing all the different r_d data on to the line (4.25) in figure 9.

The velocity of the film spreading scaled as

$$u_f \sim \frac{\Delta\sigma}{\mu_d} \left(\frac{r_d}{r_f}\right)^3 \frac{1}{4f^4}, \tag{5.2}$$

showing that the characteristic velocity of spreading is $\Delta\sigma/\mu_d$, with the spreading velocity decreasing with increasing spreading radius as r_f^{-3}. This scaling also collapsed all the velocity data obtained with different drop concentrations and r_d on to a single line $4f^4\, Ca_d = 0.5\, {r_f^*}^{-3}$ (4.26), as shown in figure 10, implying that the dependence of u_f on drop properties and r_d was adequately captured by the scaling law (5.2). Due to (5.2) and (5.1) it is also obvious that the spreading velocity showed a decrease with time as $t^{-3/4}$, before the film starts to retract at specific value of r_f.

These conclusions were verified with measurements of spreading radii obtained by the top view visualisations of ethanol-water drops spreading over a water layer, whose height was much larger than the drop radii. The visualisations showed that the spreading and eventual dissolution of the drop has many distinct stages. In the first stage, a capillary wave propagates from the point of contact of the drop with the water layer followed by an expanding circular film of ethanol-water mixture (figures 2(a) -2(c)). At some specific radius of spreading, the expanding, continuous film becomes unstable at its periphery, resulting in outward propagating fingers, while the film continues its expansion (figure 2(d)). The major part of the drop remains at the center of the film

which expands with decreasing velocity. The film starts to retract after some time, the drop thins and develops holes in it and eventually mixes with water and disappears (figures 2(g) -2(i)). From the side view visualisations, it became clear that the film originates from an initial fraction of the drop that is pulled apart in the neck expansion during coalescence of the drop with the water layer.

Based on these observations, the scaling law (5.1) was developed by combining the mass and momentum balance of the spreading film with the mass balance between the drop and the film, in which the initial fraction of the drop G appears. By calculating the flux of drop mass during the time of coalescence when the neck region retracts with capillary velocity, along with geometrical constraints, $G \approx 1/2(1 + Bo_d)^{7/6}$ was obtained as a function of the drop Bond number (4.21). The dependence of r_f on r_d, that as we saw, had a non-monotonic dependence, was thus explicitly brought into the scaling law of r_f; the resulting scaling law (5.1) then captured the non-monotonic dependence of r_f on r_d. These results were obtained for the case of film Weber number less than one so that inertial effects were neglected in the spreading of the film. The analysis was also restricted to the values of viscosity ratios $\chi = \mu_l/\mu_d < 1$ so that viscous dissipation inside the film dominates over that occurs in the underlying liquid layer. Further, the values of density ratios $\xi = \rho_l/\rho_d > 1$ was also needed so that the drop remains at the free surface while the film spreads.

Eventhough the developed scaling law satisfactorily describes the dependence of film expansion on time, drop radius and drop properties, there are still many unresolved issues in the phenomena shown by the spreading and eventual mixing of a drop on a liquid surface. The physics behind the retraction process of the film is still not clear. Same is the case about the point of transition from spreading to retraction, which in the present scaling occurs at different values of $t^*_{\mu d}$ (see figure 9). An effort to collapse the expansion, transition from expansion to retraction and the retraction, to a single curve, eventhough difficult, needs to be attempted. The physics behind the instability and the development of fingers at the periphery of a surface tension driven expanding film over a deep liquid layer is not clear; the corresponding thin layer case has been explored by many researchers (Warner *et al.* (2004) and the references therein), without yet achieving a complete understanding. The scaling in the large Weber number situation of the present case, which would presumably occur when the film viscosity is smaller than the liquid layer viscosity, with both the viscosities being low, is also still unexplored.

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Appendix A. Effect of particle concentration on surface tension

Aluminium particles are surface active and hence they change the surface tension of water. The surface tension of water laden with Aluminium particles was measured for different particle concentrations. The measurements were performed using a Sigma 700/701 force tensiometer(Biolin Scientific) using Wilhelmy plate and Du Nouy ring probes. We used particle surface densities from 0 to 78μg cm^{-2} (i.e 0 to 100 ppm) spanning the surface density of 77μg cm^{-2} (i.e 163 ppm) of particles used in the experiments. The relations between surface densities and ppm are different in visualisations and surface tension measurements since the volume to area ratio of the containers were different. Figure 11 shows that the mean surface tension, calculated from 10 repeated measurements, varies non linearly with a decrease till 15μg cm^{-2} followed by an increase till 30μg cm^{-2}. The values again drop between 30μg cm^{-2} to 45μg cm^{-2} and then stay approximately in the range 50 to 55mNm^{-1} for 45μg cm^{-2} to 80μg cm^{-2}. Similar decreasing and increasing values of surface tension with increasing particle concentrations of titanium oxide particles have been observed earlier by Dong & Johnson (2003). The initial decrease is expected to be due to decrease

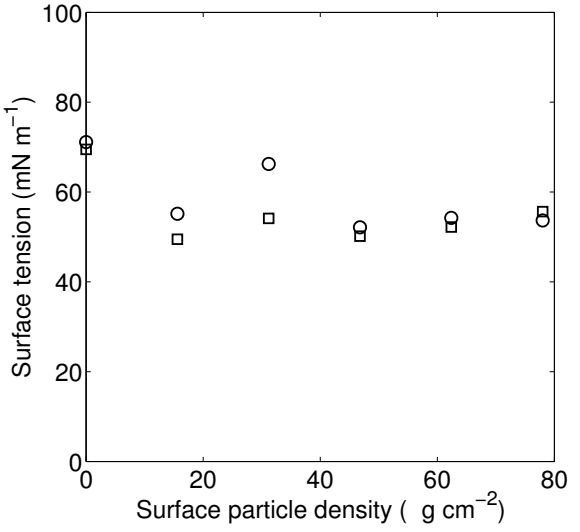

FIGURE 11. Variation of surface tension of water with surface density of Aluminium particles. ○, by Wilhelmy plate; □ by Du Nouy ring.

in free energy while the later increase to be due to capillary forces between particles (Dong & Johnson 2003). Due to this non monotonous variation, we then measured the surface tension of water with Al particles at the concentration used in visualisations many times and have now used the measured mean value of 54mNm^{-1} in all our calculations.

Appendix B. Error in r_f, t and u_f

An estimate of the error in the measurement of r_f, based on the number of pixels needed to cover the interface between the particle and the particle free regions, was 4 pixels. This number of pixels occupy a region of 0.3mm at the resolution of our imaging. Hence the maximum error possible, corresponding to our lowest r_f is 7%.

In addition to these measurement errors of r_f there is also the variation of r_f azimuthally due to the deviation of the film periphery from a circle. The range of this deviation increases as the film expands with time since instabilities start to develop at the periphery as the film expands. The range of this variation of r_f is now shown in figure 4 by showing the maximum and minimum values of r_f from the three measurements at the three azimuthal locations on the film. This range is less than the vertical shift in r_f due to the change in C_e and r_d.

The error in time measurements is due to (i) the error in frame rate as well as (ii) the error in the initial time of contact of the drop with the water surface. The error in the time of each image due to the error in FPS is negligible compared to the error in the initial time estimation. The actual instance of initial contact of the drop with the substrate could be just after the previous frame or just before the subsequent frame, from the frame which we identify as the frame at which contact occurs. Therefore the error in the initial time of contact is of the order of ± 1/fps $= \pm 0.025$s. This error in the initial time implies that the r_f vs t curves could shift by 2/fps horizontally; we show this error in the initial time as the horizontal error bars in figure 4.

Since u_f is calculated from

$$u_f = ABt^{B-1}, \tag{B 1}$$

as the derivative of the power law fit

$$r_f = At^B, \tag{B 2}$$

δu_f, the error in u_f is due to the error in the curve fit and that in t. The error in the curve fit is estimated by calculating the maximum and minimum values of A and B which will fit $r_f \pm \delta r_f$, where δr_f is the known error of 0.3 mm in r_f. From (B 1),

$$\left|\delta u_f\right| = \left|\frac{du_f}{dA}\delta A\right| + \left|\frac{du_f}{dB}\delta B\right| + \left|\frac{du_f}{dt}\delta t\right|, \tag{B 3}$$

where $\delta A, \delta B$ and δt are the errors in A, B and t. By evaluating the derivatives from (B 3) and rewriting in terms of u_f, we get

$$\left|\frac{\delta u_f}{u_f}\right| = \left|\frac{\delta A}{A}\right| + \left|\frac{\delta B}{B}\right| + \left|(B-1)\frac{\delta t}{t}\right| + \left|\delta B \ln t\right|. \tag{B 4}$$

For the case of $C_e = 100\%$ and $r_d = 0.97$mm, $A = 15.09$, $B = 0.27$, $\delta A = 0.09$, $\delta B = 0.005$, $\delta t = 0.025$s. Using these values in (B 4) at $t = 0.01$s and $u_f = 100$ mm s^{-1} we obtain 12% error in u_f. This value and the error values at two other later times are shown in figure 5.

Appendix C. Evaporation velocity

The horizontal velocity of evaporation from a horizontal film, as given by Lock(1996) is

$$U_e = \frac{\alpha_v}{L}(Ra^2 Ja^3)^{1/5}, \tag{C 1}$$

where the Jacob number, $Ja = c_{pv}\Delta T/\lambda_v$, is the ratio of sensible heat to latent heat, the Rayleigh number, $Ra = g(\Delta\rho/\rho_v)L^3/\nu_v\alpha_v$, is the ratio of buoyancy to dissipative effects, with the subscript v denoting property values of the vapour. L is the length of the film, λ the latent heat of vapourisation, ΔT and $\Delta\rho$ the temperature and density difference between the liquid surface and the ambient, c_p the specific heat at constant pressure, α the thermal diffusivity, ν the kinematic viscosity and ρ the density. By continuity, the vertical evaporation velocity is then

$$V_e = U_e\left(\frac{Ja}{Ra}\right)^{1/4} = \frac{\alpha_v}{L}\left(Ra^3 Ja^{17}\right)^{1/20} \tag{C 2}$$

Using the following properties of ethanol vapor $c_{pv} = 1400$Jkg^{-1}K^{-1}; $\nu_v = 0.835\times10^{-5}$Nsm^{-2}; $\rho_v = 0.085$kgm^{-3}; $\lambda_v = 1025\times10^3$Jkg^{-1}; $\beta = 750\times10^{-6}$°C^{-1}; $\Delta T \approx 1$°C and $\alpha_v = 0.00011$ m^{2}s^{-1} and the mean length of the film $L = 5$mm, we obtain

$$V_e \sim 4\times10^{-5}\text{ms}^{-1}, \tag{C 3}$$

which is three orders smaller than u_f.

Appendix D. Mass and momentum balance

Consider a control volume, enclosing the drop and the expanding film shown in figure 6, which deforms and expands with the film. Mass balance implies,

$$\frac{d}{dt}\left(\pi(r_f^2 - r_d^2)h_f\rho_f\right) + \frac{d}{dt}\left(\frac{4}{3}\pi r_d^3\rho_d\right) = 0. \tag{D 1}$$

Expanding the derivative, we obtain,

$$\pi r_f^2 h_f \frac{d\rho_f}{dt} - \pi r_d^2 h_f \frac{d\rho_f}{dt} + 2\pi r_f h_f \rho_f u_f + \pi r_f^2 \rho_f \frac{dh_f}{dt} - 2\pi r_d h_f \rho_f \frac{dr_d}{dt} - \pi r_d^2 \rho_f \frac{dh_f}{dt} + \frac{4}{3}\pi r_d^3 \frac{d\rho_d}{dt} + 4\pi r_d^2 \rho_d \frac{dr_d}{dt} = 0. \quad \text{(D 2)}$$

When

$$d\rho_f/dt \simeq 0,\ d\rho_d/dt \simeq 0,\ dr_d/dt \simeq 0 \text{ and } r_d \ll r_f, \quad \text{(D 3)}$$

(D 2) reduces to

$$2\pi r_f h_f \rho_f u_f + \pi r_f^2 \rho_f \frac{dh_f}{dt} = 0. \quad \text{(D 4)}$$

Similarly, momentum balance over the same control volume, implies

$$\frac{d}{dt}\left(\pi r_f^2 h_f \rho_f u_f\right) + \frac{d}{dt}\left(\frac{4}{3}\pi r_d^3 \rho_d u_d\right) = 2\pi r_f(\sigma_l - \sigma_f) - \mu_f \frac{u_f}{h_f}\pi r_f^2 \quad \text{(D 5)}$$

where u_d is the velocity inside the drop. Expanding the derivatives in (D 5) and applying (D 3), along with $du_d/dt \simeq 0$, we get

$$2\pi r_f h_f u_f^2 + \pi r_f^2 h_f \rho_f \frac{du_f}{dt} + \pi r_f^2 u_f \rho_f \frac{dh_f}{dt} = 2\pi r_f(\sigma_l - \sigma_f) - \mu_f \frac{u_f}{h_f}\pi r_f^2. \quad \text{(D 6)}$$

From (D 4), the sum of first and third terms in (D 6) is zero, resulting in

$$2\pi r_f(\sigma_l - \sigma_f) - \mu_f \frac{u_f}{h_f}\pi r_f^2 = \pi r_f^2 h_f \rho_f \frac{du_f}{dt}. \quad \text{(D 7)}$$

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